CLAIM AMENDMENTS

Amended claims: 1-13 and added new claims 14-24.

1. (Currently Amended) A process ~~Process~~ to prepare a haze free base oil having a cloud point of below 0 °C and a kinematic viscosity at 100 °C of greater than 10 cSt ~~by performing~~ comprising the following steps:

(a) hydroisomerisation of a Fischer-Tropsch synthesis product[[,]];

(b) isolating one or more fuel products and a distillation residue[[,]];

(c) reducing the wax content of the residue by contacting the feed with a hydroisomerisation catalyst under hydroisomerisation conditions[[,]]; and

(d) solvent dewaxing the product of step (c) to obtain ~~the~~ a haze free base oil.

2. (Currently Amended) The process ~~Process~~ according to claim 1, wherein the distillation residue has a 10 wt% recovery boiling point of above 500 °C and a wax content of greater than 50 wt% and wherein in step (c) the wax content is reduced to a value below 50 wt%.

3. (Currently Amended) The process according to claim 1, ~~Process according to any one of claims 1-2,~~ wherein the wax content in step (c) is reduced to below 35 wt%.

4. (Currently Amended) The process ~~Process~~ according to claim 3, wherein the wax content in the product of step (c) is between 10 and 35 wt%.

5. (Currently Amended) The process according to claim 1, ~~Process according to any one of claims 1-4,~~ wherein the Fischer-Tropsch synthesis product has a weight ratio of compounds having at least 60 or more carbon atoms and compounds having at least 30 carbon atoms in the Fischer-Tropsch product ~~is~~ of at least 0.2 and wherein at least 30 wt% of compounds in the Fischer-Tropsch synthesis product have at least 30 carbon atoms.

6. (Currently Amended) The process ~~Process~~ according to claim 5, wherein at least 50 wt% of compounds in the Fischer-Tropsch product have at least 30 carbon atoms.

7. (Currently Amended) The process according to claim 5, ~~Process according to any one of claims 5-6,~~ wherein the weight ratio of compounds having at least 60 or more carbon atoms and compounds having at least 30 carbon atoms in the Fischer-Tropsch product is at least 0.4.

8. (Currently Amended) The process according to claim 1, ~~Process according to any one of claims 1-7,~~ wherein the 10 wt% recovery boiling point of the residue as isolated in step (b) is between 350 and 550 °C.

9. (Currently Amended) The process according to claim 1, ~~Process according to any one of steps 1-8,~~ wherein more than 50 wt% of the product of step (c) boils above the 10 wt% recovery point of the residue used as feed in step (c).

10. (Currently Amended) The process ~~Process~~ according to claim 9, wherein more than 70 wt% of the product of step (c) boils above the 10 wt% recovery point of the residue used as feed in step (c).

11. (Currently Amended) The process according to claim 1, ~~Process according to any one of claims 1-10,~~ wherein the hydroisomerisation catalyst used in step (c) is a substantially amorphous based catalyst comprising a silica-alumina carrier and a noble or non-noble Group VIII metal.

12. (Currently Amended) The process according to claim 1, ~~Process according to any one of claims 1-10,~~ wherein the hydroisomerisation catalyst used in step (c) comprises a molecular sieve and a noble or non-noble Group VIII metal.

13. (Currently Amended) A process ~~Process~~ to prepare a lubricant composition not containing a viscosity modifier additive by blending a low viscosity base oil with ~~the~~ a haze free base oil ~~as obtained in step (d) of the process as described in claims 1-~~

~~12. and one or more additives~~ having a cloud point of below 0°C and a kinematic viscosity at 100°C of greater than 10 cSt prepared by a process comprising:

(a) hydroisomerisation of a Fischer-Tropsch synthesis product;

(b) isolating one or more fuel products and a distillation residue;

(c) reducing the wax content of the residue by contacting the feed with a hydroisomerisation catalyst under hydroisomerisation conditions; and

(d) solvent dewaxing the product of step (c) to obtain a haze free base oil.

14. (New) The process according to claim 13, wherein the distillation residue has a 10 wt% recovery boiling point of above 500 °C and a wax content of greater than 50 wt% and wherein in step (c) the wax content is reduced to a value below 50 wt%.

15. (New) The process according to claim 13, wherein the wax content in step (c) is reduced to below 35 wt%.

16. (New) The process according to claim 13, wherein the wax content in the product of step (c) is between 10 and 35 wt%.

17. (New) The process according to claim 13, wherein the Fischer-Tropsch synthesis product has a weight ratio of compounds having at least 60 or more carbon atoms and compounds having at least 30 carbon atoms in the Fischer-Tropsch product of at least 0.2 and wherein at least 30 wt% of compounds in the Fischer-Tropsch synthesis product have at least 30 carbon atoms.

18. (New) The process according to claim 13, wherein at least 50 wt% of compounds in the Fischer-Tropsch product have at least 30 carbon atoms.

19. (New) The process according to claim 13, wherein the weight ratio of compounds having at least 60 or more carbon atoms and compounds having at least 30 carbon atoms in the Fischer-Tropsch product is at least 0.4.

20. (New) The process according to claim 13, wherein the 10 wt% recovery boiling point of the residue as isolated in step (b) is between 350 and 550°C.

21. (New) The process according to claim 13, wherein more than 50 wt% of the product of step (c) boils above the 10 wt% recovery point of the residue used as feed in step (c).

22. (New) The process according to claim 13, wherein more than 70 wt% of the product of step (c) boils above the 10 wt% recovery point of the residue used as feed in step (c).

23. (New) The process according to claim 13, wherein the hydroisomerisation catalyst used in step (c) is a substantially amorphous based catalyst comprising a silica-alumina carrier and a noble or non-noble Group VIII metal.

24. (New) The process according to claim 13, wherein the hydroisomerisation catalyst used in step (c) comprises a molecular sieve and a noble or non-noble Group VIII metal.